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Analytical characterisation of amplitude dampening and phase-shifting in air/soil heat-exchangers

Preprint

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Abstract

This article presents the complete analytical solution for the heat diffusion of a cylindrical air/soil heat-exchanger with adiabatic or isothermal boundary condition, submitted to constant airflow with harmonic temperature signal at input. It will be shown that, depending on its thickness, the soil layer will induce either one of two kinds of amplitude-dampening and phase-shifting regimes of the periodic input signal. In particular, for a thin layer submitted to adiabatic boundary condition, it is possible to completely phase-shift the periodic input while barely dampening its amplitude, a phenomenon apparently unexploited up to now, which might give rise to interesting energy handling techniques. Analytical results are validated against a finite-difference numerical simulation model as well as against an experimental setup.

Nomenclature

Latin symbols

\[ a_s \quad \text{m}^2/\text{s} \quad \text{Thermal diffusivity of soil} \]
\[ c_a \quad \text{J/K.kg} \quad \text{Thermal capacity of air (isobaric)} \]
\[ c_s \quad \text{J/K.kg} \quad \text{Thermal capacity of soil} \]
\[ h \quad \text{W/K.m}^2 \quad \text{Amplitude-dampening exchange coefficient of air/pipe + soil} \]
\[ h_a \quad \text{W/K.m}^2 \quad \text{Convective exchange coefficient of air/pipe} \]
\[ h_s \quad \text{W/K.m}^2 \quad \text{Amplitude-dampening exchange coefficient of soil} \]
\[ h_{ss} \quad \text{W/K.m}^2 \quad \text{Amplitude-dampening exchange coefficient of soil, thickness} \delta, \text{steady-state} \]
\[ h_r \quad \text{W/K.m}^2 \quad \text{Combined amplitude-dampening and phase shifting exchange coef.} \quad (h_r^* = h_s + ik_r) \]
$k$ W/K.m$^2$ Phase-shifting exchange coefficient of air/pipe + soil

$k_s$ W/K.m$^2$ Phase-shifting exchange coefficient of soil

$m_a$ kg/s Airflow

$Nu$ --- Nusselt number

$r$ m Radial distance

$r_0$ m Radius of pipe

$R_0$ m Radius of pipe + soil

$Re$ --- Reynold's number

$t$ s Time

$S$ m$^2$ Exchange surface

$S^\delta$ m$^2$ Characteristic exchange surface for soil of thickness $\delta$, steady-state signal

$T_a$ °C Temperature of air

$T_{a0}$ °C Temperature of air at input, steady state

$T_s$ °C Temperature of soil

$T_{s0}$ °C Temperature of soil at isothermal boundary, steady state

$v_a$ m/s Velocity of air

$x$ m Length

$y$ m Width (flat heat-exchanger)

**Greek symbols**

$\delta$ m Depth of heat penetration

$\Delta h$ W/K.m$^2$ Correction on amplitude-dampening exchange coefficient of air/pipe + soil

$\Delta k$ W/K.m$^2$ Correction on phase-shifting exchange coefficient of air/pipe + soil

$\Delta R_0$ m Thickness of soil ($\Delta R_0 = R_0 - r_0$)

$\Delta t$ s Transit time within pipe

$\theta_a$ K Temperature amplitude of air

$\theta_{a0}$ K Temperature amplitude of air at input, harmonic state

$\theta_s$ K Temperature amplitude of soil, at pipe level

$\Gamma_s$ --- Temperature amplitude in soil, radial modulation

$\lambda_a$ W/K.m Thermal conductivity of air

$\lambda_s$ W/K.m Thermal conductivity of soil

$\mu_a$ kg/m.s Viscosity of air

$\rho_a$ kg/m$^3$ Density of air

$\rho_s$ kg/m$^3$ Density of soil

$\tau$ s Period of temperature oscillation

$\omega$ rad/s Frequency of temperature oscillation

**Others**

- An asterix signifies a complex value.
- A tilda signifies a dimensionless value, as defined in a specific section of the text.
1. Introduction

1.1. State of the art

To the contrary of a liquid heat storage medium, which can generally be fairly well described by means of two separate conductivity and capacity parameters (one-node model), thermal exchange with a solid medium is of diffusive nature (conduction/capacitance continuum), inducing amplitude-dampening and phase-shifting of transient temperature input which are often difficult to predict intuitively. Lacking better tools, most authors (Schiller [28], Santamouris and Lefas [26], Rodriguez and al. [25], Levit and al. [20], Seroa da Motta and Young [29], Elmer and Schiller [10], Chen and al. [6], Bansal and al. [3], Tiwari and al. [31], Athienitis and al. [2], Serres and al. [30], Tzaferis and al. [32]) are dimensioning air/soil heat exchangers by way of simple static exchange models, simple to handle but for which estimation of the fundamental parameters (air/soil heat exchange coefficient and effective soil temperature) doesn't turn out evident, especially in transient regime.

Some analytical and semi-analytical approaches which explicitly treat heat diffusion in the soil actually concern steady-state problems. An elegant, approximate solution for water driven systems by Koschenz and Lehmann [18] in fact concerns the restraint geometry of pipe networks used within thin slabs (large inter-axial pipe distance, small distance to upper and lower free surfaces) and rather pursues to compute total heat flow and mean fluid temperature than temperature at pipe exit. Using conformal mapping, another approach by Chung and al. [7] explicitly treats air driven buried pipes in a semi-infinite medium (i.e. submitted to steady thermal linking with a free upper surface, without any other geometric restriction on heat diffusion). However, apart from treating geometric configurations different from those studied in this article, such steady-state approaches unfortunately do not account for phase-shifting effects.

One of the first analytical approaches concerning periodic heat diffusion from a cylindrical in semi-infinite medium embedded pipe is proposed by Claesson and Dunand [8]. It bases on the solution
for an infinite medium, corrected by addition of a mirror sink above the free surface and yields the solution for the temperature field in the soil. The induced effect on the longitudinal temperature variation of the airflow has been completed by Sawhney and Mahajan [27], appropriate physical interpretation and operational presentation of the results unfortunately not having been carried out. Apart from the thermal link with the upper plane surface (considered way above the penetration depth and submitted to phase-shifted periodic excitation), within latter studies heat diffusion however virtually extends over an infinite region, i.e. without restriction on available soil, and does hence not allow to detect the potential of complete phase-shifting that will be put forward within this work. A similar but somehow more complex problem including the interference of neighbouring pipes is proposed by Kabashnikov and al. [17], but also concerns deeply buried pipes and doesn't either discuss the effect of phase-shifting.

All preceding analytical approaches use simplifications which will also be assumed within this work. In particular, they don't account for axial conduction within soil or for axial dispersion of fluid, as do some similar studies on single-blow techniques [21, 22], nor do they account for inhomogenous flow characteristics perpendicularly to axis.

As an alternative to the analytical approach, several numerical simulation models based on finite differences have also contributed to characterize diffusive heat exchangers. Some of them are limited to description of one only "typical" pipe (Bojic and al. [4], Mihalakakou and al. [24], Huber and Remund [16]). Other ones allow for the description of several parallel running pipes, with or without possibility to treat more complicated cases than steady flow rate, homogenous and laterally adiabatic soils, or sole sensible heat exchange (Gygli and Fort [13], Boulard and al. [5], Gauthier and al. [11], De Paepe [9]). However, when validation against monitoring is ever carried out, latter in all cases remains limited to a few hours or days and does generally not concern real scale installations, thereby not providing necessary proof of robustness one would expect. Corroboration
against an analytical solution is furthermore never given, except for the last one of these models and for the trivial case of one-dimensional heat diffusion without airflow.

Probably the most worked out finite differences numerical model is that of Hollmuller and Lachal [14], allowing for variation in airflow rate and direction, inhomogeneous soils, non-adiabatic lateral boundary conditions, as well as description of latent heat exchanges and thermal effect of charge losses. Coherent with analytical approach to be developed hereafter, lateral heat convection within a pipe section is treated by means of an overall coefficient and velocity profile is considered to be uniform, while heat diffusion in soil is treated three-dimensionally. Extensive validation against several long-term monitored real scale installations already proved good robustness [15], but as for all other models, corroboration with an analytical solution was still missing up to now.

1.2. Objectives

As a response to the preceding state of the art and as part of a wider work on air/soil heat exchangers [15], this article will treat a problem similar to that attended by Sawhney and Mahajan [27], dropping the constraint of a free upper surface, but adding an isothermal or adiabatic boundary condition at finite radial distance (limitation of available soil layer). In a first step it will be shown that, depending on its thickness, the soil layer will induce either one of two kinds of amplitude-dampening and phase-shifting regimes. In particular, for a thin layer submitted to adiabatic boundary condition, it is possible to completely phase-shift the periodic input while barely dampening its amplitude, a phenomenon apparently unexploited up to now. Latter surprising result will finally be validated against numerical simulation with the model previously developed by the author, as well as against an experimental setup.
2. Cylindrical air/soil heat-exchanger

2.1. Problem definition

We consider a constant mass flow of air (or by extension any other fluid) submitted to sinusoidal temperature oscillation at entrance of a cylindrical pipe, itself embedded in a finite cylindrical soil layer with adiabatic or isothermal boundary condition (Fig. 1). Following hypothesis will further be made:

- In relation to perpendicular heat diffusion, longitudinal one is considered to be secondary and will hence not be accounted for. As will be seen by comparison with numerical simulation, this hypothesis will be more than good enough, at least as long as the characteristic length of amplitude-dampening or phase-shifting remains larger than the natural penetration depth.

- Within a given section air is considered to be homogenous, so that the dynamic of convective air/soil heat exchange will not be described in detail but by means of a unique convective heat exchange coefficient between airflow and pipe, supposed to be constant over the whole pipe length. Velocity profile is furthermore supposed to be uniform, so that bulk and average temperatures in a pipe section can be said to coincide. Comparison with experimental data as well as with a numerical model (itself validated against several in situ monitored real scale systems) should support for these assumptions to cause negligible errors in practical applications.

- Soil thermal conductivity and capacity are considered to be homogenous and constant, variation of soil type and water content not being accounted for. Nor is being considered any water movement inducing convective heat exchange within the soil.

- The pipe itself is not taken into account. In first approximation this hypothesis could if necessary be corrected by: 1) including the conductivity of the pipe into the convective heat exchange coefficient between airflow and pipe; 2) considering an effective soil radius which takes into account the pipe's thermal capacity.

- Possible latent heat exchanges are not accounted for, which means that no water infiltration is at work and that the air temperature is supposed to remain above its dew point.
• Thermal effect of charge losses are not taken into account.

This being, perfect radial conditions as considered here do usually not arise in practical situation, so that the radial limitation should be seen as an effective radius, bearing such limitative factors as the distance between parallel running pipes (adiabatic condition) or the presence of upper/lower building/ground water (isothermal condition). We will here not seek to give general means of adequately represent a real geometry in such a simplified form, but rather to use this simplified form to derive general insight on the behaviour of air/soil heat exchangers.

2.2. Mathematical formulation

The thermal exchanges of the system are governed by the following three differential equations, which respectively describe diffusion in the soil, convective air/soil exchange and the link between both at the pipe's level:

\[
a_s \left( \frac{\partial^2 T_s}{\partial r^2} + \frac{1}{r} \frac{\partial T_s}{\partial r} \right) = \frac{\partial T_s}{\partial t}
\]

(1)

\[
c_a \dot{m}_a \left( \frac{\partial T_s}{\partial x} + \frac{1}{v_a} \frac{\partial T_s}{\partial t} \right) = 2\pi r_0 h_a \left( T_s \bigg|_{r=r_0} - T_a \right)
\]

(2)

\[
\lambda_s \left. \frac{\partial T_s}{\partial r} \right|_{r=r_0} = h_a \left( T_s \bigg|_{r=r_0} - T_a \right)
\]

(3)

Note that by appropriate rearrangement of (3), both the first equations can be written in function of \( T_s \) only, the third one yielding simple link to \( T_a \):

\[
a_s \left( \frac{\partial^2 T_s}{\partial r^2} + \frac{1}{r} \frac{\partial T_s}{\partial r} \right) = \frac{\partial T_s}{\partial t}
\]

(4)

\[
\left( \frac{\partial}{\partial x} + \frac{1}{v_a} \frac{\partial}{\partial t} \right) \left( T_s - \frac{\lambda_s}{h_a} \frac{\partial T_s}{\partial r} \right) \bigg|_{r=r_0} - \frac{2\pi r_0}{c_a \dot{m}_a} \lambda_s \left. \frac{\partial T_s}{\partial r} \right|_{r=r_0} = 0
\]

(5)
\[ T_a = \left( T_s - \frac{\lambda_s}{h_a} \frac{\partial T_s}{\partial r} \right)_{r=R_0} \]  

(6)

Dependence of \( a_s \) and \( v_a \) on other parameters is given by:

\[ a_s = \frac{\lambda_s}{c_s \rho_s} \]  

(7)

\[ v_a = \frac{\dot{m}_a}{\rho_a \pi r_0^2} \]  

(8)

while that of \( h_a \) will depend on the value of the Reynolds number:

\[ Re = \frac{\rho_a v_a}{\mu_a} 2r_0 \]  

(9)

For laminar flow \( h_a \) may be considered to be independent of \( Re \) and thus of air velocity, which is not the case for turbulent flow anymore [19]:

\[ h_a = \frac{\lambda_a}{2r_0} Nu \quad \text{with} \quad Nu = \begin{cases} 4.36 \quad (Re < 2'300) \\ 0.023Re^{0.8} Pr^{0.33} \quad (Re > 10'000) \end{cases} \]  

(10)

A refined formulation of latter form is also developed by Gnielinski [12], taking into account length to diameter as well as air to pipe temperature ratios, whereas for engineering purposes a roughly accurate linear form in function of \( v_a \) may also be used [15].

Finally, soil boundary condition will be either isothermal or adiabatic:

\[ T_s \big|_{r=R_0} = T_s0 \quad \text{or} \quad \frac{\partial T_s}{\partial r} \big|_{r=R_0} = 0 \]  

(11)

and input air temperature is considered to be of a steady harmonic form:

\[ T_a \big|_{x=0} = T_{a0} + \theta_{a0} \cos(\omega x) \]  

(12)

Keeping in mind the linearity of (4-6), which allows for addition of distinct conditions / solutions, we will however seek separate solutions for the steady input (driven by \( T_{a0} \) and eventually \( T_s0 \)) and for the harmonic component (driven by \( \theta_{a0} \)).
2.3. Steady-state case

Before dealing with the periodic case we are most interested in, we will solve the steady-state, whose resolution as well as result will be used as a reference case. It is defined by following input and boundary conditions:

\[ T_a\big|_{x=0} = T_{a0} \]  \hspace{1cm} (13)

\[ T_s\big|_{r=R_0} = T_{s0} \hspace{1cm} \text{or} \hspace{1cm} \frac{\partial T_s}{\partial r}\big|_{r=R_0} = 0 \]  \hspace{1cm} (14)

Uncoupling of geometric components

In steady state regime \( T_s \) and \( T_a \) do not depend on \( t \) and we may proceed by separation of radial and longitudinal components, as follows:

\[ T_s(x,r) = T_{s0} + \theta_s(x) \cdot \Gamma_s(r) \]  \hspace{1cm} (15)

\[ T_a(x) = T_{a0} + \theta_a(x) \]  \hspace{1cm} (16)

Since \( \theta_s \) and \( \Gamma_s \) are not defined in a unique way (multiplication by any constant and its inverse constituting another set of solution), we may arbitrarily impose following additional condition:

\[ \Gamma_s\big|_{r=r_0} = 1 \]  \hspace{1cm} (17)

which fixes \( \theta_s \) as being the pipe temperature (temperature of the soil at \( r = r_0 \)).

Using (15-16) and further defining:

\[ h_r = \lambda \left( -\frac{1}{\Gamma_s} \frac{d\Gamma_s}{dr} \right) \bigg|_{r=R_0} \]  \hspace{1cm} (18)

the original system (4-6) then writes as follows:

\[ \frac{\partial^2 \Gamma_s}{\partial r^2} + \frac{1}{r} \frac{\partial \Gamma_s}{\partial r} = 0 \]  \hspace{1cm} (19)

\[ \frac{\partial \theta_s}{\partial x} + \frac{2\pi r_0}{c_s \bar{m}_s} h_s h_r \cdot \theta_s = 0 \]  \hspace{1cm} (20)
\[ \theta_s = \frac{h_s + h_t}{h_s} \cdot \theta_s \]  

(21)

boundary conditions (13-14) becoming:

\[ \theta_s \bigg|_{x=0} = T_{s0} - T_{t0} \]  

(22)

\[ \Gamma_s \bigg|_{r=R_0} = 0 \quad \text{or} \quad \frac{d\Gamma_s}{dr} \bigg|_{r=R_0} = 0 \]  

(23 a/b)

**Longitudinal solution**

Trivial solution of (20), its link to (21) and boundary condition (22) allow to determine following longitudinal solutions:

\[ \theta_s(x) = \frac{h_s}{h_s + h_t} (T_{s0} - T_{t0}) \exp \left( -\frac{2\pi r_0}{c_s m_a} \frac{h_s h_t}{h_s + h_t} x \right) \]  

(24)

\[ \theta_a(x) = (T_{s0} - T_{t0}) \exp \left( -\frac{2\pi r_0}{c_s m_a} \frac{h_s h_t}{h_s + h_t} x \right) \]  

(25)

**Radial solution**

Submitted to condition (17), the general solution of (19) can be written as:

\[ \Gamma_s(r) = \frac{\ln(Ar)}{\ln(Ar_0)} \]  

(26)

where \( A \) is to be determined by one of the radial boundary conditions (23 a/b).

- With the isothermal condition (23 a) \( A = R_0 \), so that (26) and (18) become

\[ \Gamma_s(r) = \frac{\ln \left( \frac{r}{R_0} \right)}{\ln \left( \frac{r_0}{R_0} \right)} \]  

(27 a)

\[ h_t = \frac{\lambda_s}{r_0 \ln \left( \frac{R_0}{r_0} \right)} \]  

(28 a)
• With the adiabatic condition (19 b) \( A \) tends to infinity, so that (26) and (18) become

\[
\Gamma_s (r) = 1 \quad (27 \text{ b})
\]
\[
h_r = 0 \quad (28 \text{ b})
\]

**Complete solution**

Defined by (15-16), the complete solution finally writes as the product of the partial solutions (24-25) and (27):

• With an isothermal boundary condition, one gets an exponential dampening of the input signal:

\[
T_a (x) = T_{s0} + (T_{a0} - T_{s0}) \exp\left(-\frac{2\pi r_0}{c_a m_a} h x\right) \quad (29)
\]

where the effective exchange coefficient \( h \) is given by serial linking of the convective and diffusive resistances of air and soil:

\[
h = \frac{h_a h_s}{h_a + h_s} \quad (30)
\]

and where the diffusive soil coefficient \( h_s \) is given by identification with \( h_r \) (28 a).

With its thermal tension divided by the presence of \( h_a \), the same exponential dampening arises along the soil, linked to a radial dampening of logarithmic type:

\[
T_s (x, r) = T_{s0} + \frac{h_a}{h_s + h_s} \ln\left(\frac{r}{r_0}\right) \cdot (T_{a0} - T_{s0}) \exp\left(-\frac{2\pi r_0}{c_a m_a} h x\right) \quad (31)
\]

• With an adiabatic boundary condition, one gets the trivial solution:

\[
T_a (x) = T_s (x, r) = T_{a0} \quad (32)
\]

corresponding to thermal saturation of the soil, which doesn't exchange anything with the airflow anymore.
2.4. Harmonic case

The harmonic case is on its turn defined by following input and boundary conditions:

\[ T_a \big|_{x=0} = \theta_{a0} \cos(\omega t) \]  

\[ T_s \big|_{r=R_0} = 0 \quad \text{or} \quad \frac{\partial T_s}{\partial r} \bigg|_{r=R_0} = 0 \]  

It can be solved much in the same manner as before.

Uncoupling of time and geometric components

In harmonic steady state regime we will seek a solution by using a complex notation:

\[ T_a = \text{Re} \left[ \theta_a^*(x) \exp(i\omega t) \right] \]  

\[ T_s = \text{Re} \left[ \theta_s^*(x) \Gamma_s^*(r) \exp(i\omega t) \right] \]  

which enables formal uncoupling of space and time variables, phase-shifts being carried by the argument of complex amplitudes \( \theta_a^* \), \( \theta_s^* \) and \( \Gamma_s^* \). Again we will fix \( \theta_s^* \) to be the pipe's temperature, by imposing following additional condition:

\[ \Gamma_s^* \big|_{r=R_0} = 1 \]  

and will define:

\[ h_l = \lambda \left( -\frac{1}{\Gamma_s^*} \frac{d\Gamma_s^*}{dr} \right) \bigg|_{r=R_0} \]  

The original system (4-6) then be writtes as follows:

\[ \frac{\partial^2 \Gamma_s^*}{\partial r^2} + \frac{1}{r} \frac{\partial \Gamma_s^*}{\partial r} = i \frac{\omega}{a_s} \Gamma_s^* \]  

\[ \frac{\partial \theta_s^*}{\partial x} + \left( i \frac{\omega}{v_a} + \frac{2\pi r_0}{c_a h_a} \frac{h_a h_l^*}{h_a + h_l} \right) \cdot \theta_s^* = 0 \]  

\[ \theta_a^* = \frac{h_a + h_l^*}{h_a} \cdot \theta_s^* \]  

boundary conditions (33-34) becoming:
\[ \theta^*_{a} \big|_{x=0} = \theta_{a0} \]  \hspace{1cm} (42)

\[ \Gamma^*_{s} \big|_{r=R_0} = 0 \quad \text{or} \quad \frac{d\Gamma^*_{s}}{dr} \bigg|_{r=R_0} = 0 \]  \hspace{1cm} (43 \text{a/b})

**Longitudinal solution**

Just as before, trivial solution of (40), its link to (41) and boundary condition (42) allow to determine following longitudinal solutions:

\[ \theta^*_{l}(x) = \frac{h_a}{h_a + h_{r}} \theta_{a0} \exp \left( -i \omega \Delta t - \frac{2 \pi \sigma}{c_a \hat{m}_a} \frac{h_a h_{r}}{h_a + h_{r}} \right) \]  \hspace{1cm} (44)

\[ \theta^*_{a}(x) = \theta_{a0} \exp \left( -i \omega \Delta t - \frac{2 \pi \sigma}{c_a \hat{m}_a} \frac{h_a h_{r}}{h_a + h_{r}} \right) \]  \hspace{1cm} (45)

where \( \Delta t \) represents the transit time of the airflow over distance \( x \):

\[ \Delta t = \frac{x}{v_{a}} \]  \hspace{1cm} (46)

**Radial solution**

The general solution of (39) can be written as:

\[ \Gamma^*_{s}(r) = A_f I_0 \left( 1 + i \right) \frac{r}{\delta} + A_k K_0 \left( 1 + i \right) \frac{r}{\delta} \]  \hspace{1cm} (47)

where \( \delta \) represents the penetration depth proper to the soil diffusivity and the signal frequency:

\[ \delta = \sqrt{\frac{2a_r}{\omega}} = \sqrt{\frac{a_r \tau}{\pi}} \]  \hspace{1cm} (48)

and where \( I_n \) and \( K_n \) are modified Bessel functions of order \( n \) (Abramowitz and Stegun [1]). Using the derivation rules for Bessel functions, coefficients \( A_f \) and \( A_k \) are determined by means of (37) and one of the boundary conditions (43 a/b). By further use of (38) one finally gets:

- With the isothermal condition (43 a):
\[
\begin{align*}
\Gamma^*_s(r) &= \frac{I_0 \left(1 + i \frac{r}{\delta}\right) \cdot K_0 \left(1 + i \frac{R_0}{\delta}\right) - K_0 \left(1 + i \frac{r}{\delta}\right) \cdot I_0 \left(1 + i \frac{R_0}{\delta}\right)}{I_0 \left(1 + i \frac{r_0}{\delta}\right) \cdot K_0 \left(1 + i \frac{R_0}{\delta}\right) - K_0 \left(1 + i \frac{r_0}{\delta}\right) \cdot I_0 \left(1 + i \frac{R_0}{\delta}\right)} \\
&= \frac{I_0 \left(1 + i \frac{r}{\delta}\right) \cdot K_0 \left(1 + i \frac{R_0}{\delta}\right) + K_0 \left(1 + i \frac{r_0}{\delta}\right) \cdot I_0 \left(1 + i \frac{R_0}{\delta}\right)}{I_0 \left(1 + i \frac{r_0}{\delta}\right) \cdot K_0 \left(1 + i \frac{R_0}{\delta}\right) + K_0 \left(1 + i \frac{r_0}{\delta}\right) \cdot I_0 \left(1 + i \frac{R_0}{\delta}\right)}
\end{align*}
\]

(49 a)

\[
\begin{align*}
h^*_r &= \frac{\lambda}{\delta} \cdot (1 + i) \cdot (-1) \cdot \frac{I_1 \left(1 + i \frac{r_0}{\delta}\right) \cdot K_0 \left(1 + i \frac{R_0}{\delta}\right) - K_1 \left(1 + i \frac{r_0}{\delta}\right) \cdot I_0 \left(1 + i \frac{R_0}{\delta}\right)}{I_0 \left(1 + i \frac{r_0}{\delta}\right) \cdot K_0 \left(1 + i \frac{R_0}{\delta}\right) + K_0 \left(1 + i \frac{r_0}{\delta}\right) \cdot I_0 \left(1 + i \frac{R_0}{\delta}\right)} \\
&= \frac{\lambda}{\delta} \cdot (1 + i) \cdot (-1) \cdot \frac{I_1 \left(1 + i \frac{r_0}{\delta}\right) \cdot K_1 \left(1 + i \frac{R_0}{\delta}\right) + K_1 \left(1 + i \frac{r_0}{\delta}\right) \cdot I_1 \left(1 + i \frac{R_0}{\delta}\right)}{I_0 \left(1 + i \frac{r_0}{\delta}\right) \cdot K_1 \left(1 + i \frac{R_0}{\delta}\right) + K_1 \left(1 + i \frac{r_0}{\delta}\right) \cdot I_1 \left(1 + i \frac{R_0}{\delta}\right)}
\end{align*}
\]

(50 a)

- With the adiabatic condition (43 b):

\[
\begin{align*}
\Gamma^*_s(r) &= \frac{I_0 \left(1 + i \frac{r}{\delta}\right) \cdot K_1 \left(1 + i \frac{r_0}{\delta}\right) + K_0 \left(1 + i \frac{r}{\delta}\right) \cdot I_1 \left(1 + i \frac{r_0}{\delta}\right)}{I_0 \left(1 + i \frac{r_0}{\delta}\right) \cdot K_0 \left(1 + i \frac{r_0}{\delta}\right) + K_0 \left(1 + i \frac{r_0}{\delta}\right) \cdot I_1 \left(1 + i \frac{r_0}{\delta}\right)} \\
h^*_r &= \frac{\lambda}{\delta} \cdot (1 + i) \cdot (-1) \cdot \frac{I_1 \left(1 + i \frac{r_0}{\delta}\right) \cdot K_1 \left(1 + i \frac{R_0}{\delta}\right) - K_1 \left(1 + i \frac{r_0}{\delta}\right) \cdot I_1 \left(1 + i \frac{R_0}{\delta}\right)}{I_0 \left(1 + i \frac{r_0}{\delta}\right) \cdot K_1 \left(1 + i \frac{R_0}{\delta}\right) + K_1 \left(1 + i \frac{r_0}{\delta}\right) \cdot I_1 \left(1 + i \frac{R_0}{\delta}\right)}
\end{align*}
\]

(49 b)

(50 b)

**Complete solution:**

Defined by (35-36), the complete solution finally writes as the product of the partial solutions (44-45) and (49), of which only the real part should be taken. Hence, after decomposition in real and imaginary parts of the link which occurs between \(h_a\) and \(h^*_r\):

\[
\frac{h_a h^*_r}{h_a + h^*_r} = h + i k
\]

the air output temperature in steady state oscillation can explicitly be written in terms of amplitude-dampening and phase-shifting of the input signal:

\[
T_a(x, t) = \theta_{a_0} \cdot \exp \left( -\frac{2\pi r_0}{c_a \dot{m}_a} hx \right) \cdot \cos \left( \omega(t - \frac{x}{v_a}) - \frac{2\pi r_0}{c_a \dot{m}_a} kx \right)
\]

(52)

Explicit evaluation of the coefficients \(h\) and \(k\) in (46) occurs by decomposition of \(h^*_r\) in real and imaginary parts:
\[ h'_v = h_s + ik_s \]  

(53)

which can be done by substituting the Bessel functions occurring in (50) by their approximating 
series (Abramowitz and Stegun, [1]). With this definition, (51) may explicitly be written as follows:

\[
h = \frac{h_u h_s}{h_u + h_s} + \Delta h
\]

(54)

\[
k = \frac{h_u k_s}{h_u + h_s} + \Delta k
\]

(55)

\[
\Delta h = (+) \frac{h_u^2 k_s^2}{(h_u + h_s)(h_u^2 + 2h_u h_s + h_s^2 + k_s^2)} \quad \text{with } \lim_{h_s \to 0} \Delta h = 0
\]

(56)

\[
\Delta k = (-) \frac{h_u k_s (h_u h_s + h_s^2 + k_s^2)}{(h_u + h_s)(h_u^2 + 2h_u h_s + h_s^2 + k_s^2)} \quad \text{with } \lim_{h_s \to 0} \Delta k = 0
\]

(57)

At least in case of good convective heat exchange (large values of \( h_u \)), the amplitude-dampening 
coefficient \( h \) hence essentially turns out to be determined by serial linking of the convective 
coefficient \( h_u \) with the diffusive coefficients \( h_s \), while a very similar relation between \( h_u \), \( h_s \) and \( k_s \) 
determines the phase-shifting coefficient \( k \).

### 2.5. Dimensionless values

In order to analyse these parameters in a synthetic way, it will be useful to define following 
dimensionless values, which we classify by type:

\[
\tilde{T}_u = \frac{T_u}{\theta_{a0}}
\]

(58)

\[
\tilde{t} = \frac{t}{\tau}, \quad \Delta \tilde{t} = \frac{\Delta t}{\tau}
\]

(59)

\[
\tilde{r}_0 = \frac{r_0}{\delta}, \quad \Delta \tilde{R}_0 = \frac{\Delta R_0}{\delta}
\]

(60)

\[
\tilde{S} = \frac{S}{S_d}
\]

(61)
\[ \bar{h}_s = \frac{h_s}{h_\delta}, \quad \bar{k}_s = \frac{k_s}{h_\delta}, \quad \bar{h}_a = \frac{h_a}{h_\delta}, \quad \bar{k} = \frac{k}{h_\delta}, \quad \Delta \bar{h} = \frac{\Delta h}{h_\delta}, \quad \Delta \bar{k} = \frac{\Delta k}{h_\delta} \]  

(62)

where \( S \) represents the air/tube exchange surface:

\[ S = 2\pi r_0 x \]  

(63)

and where, accordingly to (28-30), \( h_\delta \) and \( S_\delta \) are the diffusive exchange coefficient and associated characteristic surface for a steady signal, a soil layer of thickness \( \delta \) and an infinite convection coefficient \((h = h_s = h_\delta)\):

\[ h_\delta = \frac{\lambda_s}{r_0 \ln \left(1 + \frac{\delta}{r_0}\right)} \]  

(64)

\[ S_\delta = \frac{c_s m_a}{h_\delta} \]  

(65)

With these definitions (52) finally reduces to:

\[ \tilde{T}_a = \exp\left(-\bar{h}\tilde{S}\right) \cdot \cos\left(2\pi\left(\tilde{t} - \Delta\tilde{t}\right) - k\tilde{S}\right) \]  

(66)

2.6. Diffusive coefficients \( h_s \) and \( k_s \)

By means of these reductions, the behaviour of the diffusive coefficients \( h_s \) and \( k_s \) in function of the soil thickness \( \Delta R_0 \) reveals their physical meaning (Fig. 2).

![Fig. 2](image)

In case of an isothermal boundary condition, increase of soil thickness \( \Delta R_0 \) progressively isolates the pipe from the temperature source at the surface, which translates by a decrease of dampening coefficient \( h_s \) (with the same logarithmic behaviour (28a) as for steady input). Latter coefficient however stabilises as the soil thickness exceeds \( \delta \), indicating that the active layer now restricts to the penetration depth, exceeding soil basically remaining unaffected by the temperature oscillation of the air.
A similar limitation by $\delta$ can be observed for an adiabatic boundary condition: above a thickness $\delta$ oscillatory behaviour of the input signal induces dampening just in the same manner as for an isothermal boundary condition (and much to the contrary of the flat behaviour (28b) of steady input). As a matter of fact, if the boundary condition is situated beyond the oscillatory penetration depth, there is no way for the air to "distinguish" whether latter condition is adiabatic or isothermal. Should the soil thickness $\Delta R_0$ however drop below $\delta$, then the dampening coefficient $h_s$ would decrease and eventually vanish, indicating that the thermal capacity is being reduced, the limiting case being that of a perfectly isolated pipe with no active mass whatsoever.

Similar saturation phenomena appears for the phase-shifting coefficient $k_s$. For one or the other boundary conditions, latter rises along with $\Delta R_0$ and stabilises as latter goes beyond penetration depth $\delta$ (in the case of an adiabatic boundary condition first going through a maximum point). To the contrary of the dampening coefficient $h_s$ whose stabilising value is independent of the pipe radius (in dimensionless form!), that of $k_s$ turns out to decrease along with the radius though.

### 2.7. Convective coupling and corrective coefficients $\Delta h$ and $\Delta k$

In case of an adiabatic boundary conditions, coupling with a finite convective coefficient $h_a$ essentially acts by dividing the thermal potential, so that effective coefficients $h$ and $k$ basically behave like reduced forms of $h_s$ and $k_s$ (Fig. 3), which justifies formulation (49-50). When $h_a$ decreases close to $h_\delta$ or smaller, corrective coefficients $\Delta h$ and $\Delta k$ can become quite important though (Fig. 4), especially for $\Delta R_0$ smaller than $\delta$. In latter case $\Delta h$ will tend to linearise the power-behaviour of $h$ in a way similar to that of $k$, which will perturb the phase-shifting phenomena put forward in next section.

Less important for subsequent considerations, similar discussion of the isothermal case is to be found in [15].
2.8. Flat heat-exchanger

By proper geometric modification of governing equations (1-3), foregoing study can be extended to the case of a flat heat-exchanger (convection between an airflow and a flat plate of length $x$, width $y$ and finite thickness $\Delta R_0$, with induced one-dimensional heat diffusion along $r$, perpendicular to airflow):

$$a_s \frac{\partial^2 T_s}{\partial r^2} = \frac{\partial T_s}{\partial t}$$  \hspace{1cm} (67)

$$c_a \dot{m}_a \left( \frac{\partial T_a}{\partial x} + \frac{1}{v_a} \frac{\partial T_a}{\partial t} \right) = yh_a (T_s|_{r=0} - T_a)$$  \hspace{1cm} (68)

$$\lambda_s \frac{\partial T_s}{\partial r} \bigg|_{r=0} = h_a (T_s|_{r=0} - T_a)$$  \hspace{1cm} (69)

For a harmonic input of type (33), resulting output air temperature turns out to be of equivalent form as (52):

$$T_a(x,t) = \theta_{a0} \cdot \exp \left( - \frac{S}{c_a \dot{m}_a} \right) \cdot \cos \left( \omega (t - \frac{x}{v_a} - \frac{S}{c_a \dot{m}_a} \right)$$  \hspace{1cm} (70)

where $S = xy$ represents the air/plate exchange surface. Coefficients $h$ and $k$ continue to be determined by (53-57), where $h^*_f$ is now given as follows:

- With an isothermal boundary condition at $\Delta R_0$:

$$h^*_f = \frac{\lambda}{\delta} \cdot (1 + i) \cdot \frac{\cosh{(1 + i) \frac{\Delta R_0}{\delta}}}{\sinh{(1 + i) \frac{\Delta R_0}{\delta}}}$$  \hspace{1cm} (71 a)

- With an adiabatic boundary condition at $\Delta R_0$:

$$h^*_f = \frac{\lambda}{\delta} \cdot (1 + i) \cdot \frac{\sinh{(1 + i) \frac{\Delta R_0}{\delta}}}{\cosh{(1 + i) \frac{\Delta R_0}{\delta}}}$$  \hspace{1cm} (71 b)
Coherent with the fact that a flat heat exchanger actually corresponds to a finite portion of a hollow cylinder of thickness $\Delta R_0$ and infinite radius $r_0$, expression (71) actually turns out to coincide with the limiting form of (50), so that $h_s$ and $k_s$ can also be evaluated by means of Fig. 2 with $r_0 = 100\delta$.

3. Amplitude-dampening versus phase-shifting

Solution (52) or (70) clearly show the joint amplitude-dampening and phase-shifting a diffusive heat-exchanger exerises on an airflow with oscillatory input signal. We will now analyse the relative importance of these two effects, distinguishing soil layers sufficiently or insufficiently thick for heat diffusion to expand over all its natural depth.

3.1. Amplitude dampening by complete development of the active layer

With a sufficiently thick soil ($\Delta R_0 > \delta$) isothermal and adiabatic boundary conditions have been seen to have equivalent effects on the airflow temperature. The dampening coefficient $h_s$ is then essentially equivalent to the dampening coefficient $h_\delta$ for a steady-state input and a soil of thickness $\delta$, while the phase-shifting coefficient $k_s$ generally remains below that value, which is only reached in the case of a flat exchanger. Compared to amplitude-dampening, phase shifting will thus become a relatively secondary phenomenon.

Hence (Fig. 5, left), for a flat exchanger and a sufficiently good convective coupling ($h_a > 10 h_\delta$), an exchange surface $S = S_\delta$ will yield a phase shift of barely 1 rad (4 hours in daily frequency, 2 months in annual frequency) for an amplitude dampening by a factor $e^{-1}$. Complete phase shifting of $\pi$ (12 hours, respectively 6 months) will only be reached when the amplitude already dampened down by a factor $e^{-\pi} \sim 4\%$. Other geometric cases will be characterised by an even smaller phase-shift, as $k$ decreases along with the pipe radius as well as with the convective exchange $h_a$ (Fig. 3).
3.2. Phase-shifting by development of a thin isolated layer

Only when the soil thickness reduces beneath $\delta$ will isothermal and adiabatic condition differ from each other. In the first case, the airflow entering in closer contact with the constant temperature source, amplitude dampening will turn out even stronger, to the contrary of phase-shifting which will decrease even more (Fig. 2).

For the adiabatic case, a completely new phenomenon will however appear. Although both diffusive coefficients then progressively drop to zero along with $\Delta R$, $k_s$ does it in a linear while $h_s$ in a power form (Fig. 2). As a result, for a value of $\Delta R$ close to $0.2\delta$ there is a residual phase-shifting coefficient, all the more important as the pipe radius also is (up to $0.4 h_\delta$ in case of a flat exchanger), for an almost extinguished dampening coefficient. Supposing a fairly good convective exchange it hence becomes possible, with such a thin and isolated layer configuration, to get a complete phase-shift of the input oscillation with almost no amplitude dampening (Fig. 5, right). As has been seen before, poor convective exchange however will linearise the form of $h$, amplitude-dampening becoming close to or stronger than phase-shifting again.

To the contrary of preceding amplitude-dampening regime (which is usually striven for when preheating or cooling of air by means of air/soil heat exchangers), this phase-shifting regime seems not to have been identified or intentionally used ever before.

4. Validation

4.1. Numerical simulation

First validation as well as illustration of the results just discussed will be given on the example of a theoretical air-to-earth heat exchanger used for preheating or cooling of air taken from ambient.
Input is the standard annual meteorological data for Geneva as given in hourly time step by the Meteonorm database [23].

The analysed system is composed of a 25 cm diameter pipe embedded in a sandy and weakly saturated soil cylinder (conduction and capacity of 1.9 W/K.m and 1.9 MJ/K.m$^3$, yielding 17 cm and 3.2 m daily and annual penetration depths), with adiabatic boundary conditions and submitted to a constant 200 kg/h airflow (inducing a value of $h_a$ of 4.6 W/K.m$^2$). By Fourier analysis of the input temperature into a complete sum of harmonics (from yearly up to hourly frequency), the analytical output is being reconstructed for a set of 3 geometric configurations (Tab. 1), yielding respectively (Fig. 6) : a) dampening of annual amplitude ; b) dampening of daily amplitude ; c) phase-shifting of annual amplitude.

Validation concerns output from a finite element simulation model previously developed by the author and briefly described in the introduction. Input temperature, airflow, overall convective exchange coefficient, as well as soil properties were set to same values as above. Rectangular meshing was chosen so as to yield equivalent cylindrical sections than analytical problem (at pipe as well as soil level). It was laterally submitted to adiabatic boundary condition and longitudinally segmented in 1 m pieces. Finally, so as to determine the effect of longitudinal heat diffusion, not taken into account in the analytical model, latter segments alternatively were or weren’t separated with a 10 cm super-isolating layer (2.8 $10^{-5}$ W/K.m conductivity, 2.8 kJ/m$^3$ capacity).

| Tab. 1 + Fig. 6 |

Despite the rectangular approximation of the numerical model, an excellent correspondence with the analytical approach is manifest (Fig. 6 and Tab. 1), with a mean bias of at most 0.5 K and a standard deviation below 0.2 K. At least for these configurations, with characteristic lengths way
higher than annual and daily penetration depths, weak effect of longitudinal diffusion is moreover testified by the quasi equivalence of numerical results with axial diffusion turned on or off.

4.2. Experimental setup

Preliminary experimental validation of 12 hour phase-shifting was done on a flat heat exchanger (5 mm air strip between two corrugated concrete plates 3.4 cm thick, 25 cm large and 2 m long, with 12 cm lateral polystyrene insulation), submitted to an 8 m³/h airflow (Fig. 7). At input, weak meteorological oscillation was boosted with a 12 hour electrical heating pulse (Fig. 8).

Despite too weak a convective exchange (inducing non-negligible amplitude-dampening) and too small an exchange surface (inducing not more than an 8 hour phase-shift), there is clear evidence of the phenomenon striven for. This experiment furthermore shows the critical importance of the active layer, in present case chosen so as to phase-shift the fundamental frequency, while all higher frequencies of the "square" pulse are being dampened out.

Finally, monitored data can be fairly well reproduced by way of analytically reconstructed output (Fig. 8), having in mind that Fourier decomposition also assumes the repeated periodic pattern as a historical input. This analytical reconstruction however critically depends on the value of \( h_a \), best results here being obtained with \( h_a = 17 \pm 2 \text{ W/K.m}^2 \) (for \( \lambda_s = 1.5 \text{ W/K.m} \) and \( c_s = 2.6 \text{ MJ/K.m}^3 \)). Such an experimental setup could hence also be used for experimental determination of convective exchange coefficients, as here with corrugated plates.
5. Conclusions

We developed an analytical solution for a cylindrical (or flat) air/soil heat-exchanger submitted to constant airflow, with harmonic temperature input and adiabatic or isothermal boundary condition, yielding following results:

- Characterisation and physical interpretation of amplitude-dampening and phase-shifting phenomena which, depending on the available soil thickness, are subject to distinct regimes. Depending on the effect striven for and the frequency of interest, this characterisation sets up the basis for proper dimensioning of air/soil heat exchangers.

- Detection of the possibility to use a diffusive heat-exchanger for phase-shifting of a temperature oscillation, with almost no amplitude-dampening. Apparently unexploited up to now, this phenomena might give rise to interesting energy handling techniques, on air as well as maybe on water driven systems. Yearly phase-shifting of ambient temperature as presented in this article probably would turn out to be technically unrealistic (size, adiabatic conditions) and should be perturbed by latent exchanges (as can be shown with numerical simulation taking into account air humidity). Daily phase-shifting for summer cooling purposes should however be an interesting option, on which work at the Centre universitaire d'étude des problèmes de l'énergie is currently being developed.

- Numerical validation on hourly data over one year confirms the analytical results and the coherence of subjacent assumptions, at least in the range of tested configurations. Experimental validation of daily phase-shifting, which also contributes to settle analytical results, could further be used for precise determination of effective convective heat exchange coefficient within air/soil heat-exchangers.

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We wish to thank Bernard LACHAL from the Centre universitaire d'étude des problèmes de l'énergie for suggesting to treat the analytical problem of air/soil heat-exchangers and for constant
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Bibliography


Fig. 1: Schematic of cylindrical air/soil diffusive heat exchanger.
Fig. 2: Diffusive amplitude-dampening and phase-shifting coefficient in function of soil thickness and different pipe radius.
Fig. 3: amplitude-dampening and phase-shifting coefficient, adiabatic boundary condition.
Fig. 4: Total amplitude-dampening and phase-shifting coefficient-correction, adiabatic boundary condition.
Fig. 5: Amplitude-dampening and phase-shifting of periodic input in flat air/soil heat-exchanger with adiabatic boundary condition.
Fig. 6 : Some configurations of cylindrical air/soil heat-exchangers with adiabatic boundary condition: daily extremes over one year for hourly input from ambient and analytically computed output (left) and hourly deviation from numerical simulation model (right).
Fig. 7: Experimental setup for phase-shifting with controlled amplitude-dampening: a) basis: washed concrete plate on polystyrene insulation; b) air strip and second concrete plate; c) finish (before lateral and upper insulation): air injection, air tightness and monitoring apparatus
Fig. 8 Validation of phase-shifting with controlled amplitude-dampening.
### Tab. 1: Some configurations of cylindrical air/soil heat-exchangers with adiabatic boundary condition: amplitude-dampening and phase-shifting parameters as well as mean deviations from numerical simulation model.

<table>
<thead>
<tr>
<th>configuration</th>
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<th>axial diff. on</th>
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<td>annual</td>
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<td>$\overline{S_h}$</td>
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1) mean difference (numerical – analytical).
2) square root of mean square difference (after deduction of bias).